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### **TECHNICAL MEMORANDUM**

### **NON-TIME-CRITICAL REMOVAL ACTION**

## BEEDE WASTE OIL SITE PLAISTOW, NEW HAMPSHIRE

## RESPONSE ACTION CONTRACT (RAC), REGION I

For U.S. Environmental Protection Agency

By Tetra Tech NUS, Inc.

EPA Contract No. 68-W6-0045 EPA Work Assignment No. 105-NARV-011T TtNUS Project No. N4103

January 2005



TETRA TECH NUS, INC.

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Diane M. Baxter Project Manager

in M Baxti

George D. Gardner, P.E

Program Manager

# TABLE OF CONTENTS TECHNICAL MEMORANDUM NON-TIME-CRITICAL REMOVAL ACTION BEEDE WASTE OIL SITE PLAISTOW, NEW HAMPSHIRE

SECTIO	<u>n</u>	PAGE
1.0	INTRODUCTION	1
2.0	NTCRA WASTE EXTRACTION EVALUATION	1
3.0	OIL THICKNESS EVALUATION	3
4.0	OIL VOLUME EVALUATION	5 8
	TABLES	

#### <u>NUMBER</u>

- Oil and Emulsion Analytical Results Detected Compounds Only
- 2 LNAPL Emulsion Composition

#### **FIGURES**

#### **NUMBER**

- 1 Cumulative Oil and Water Extracted through September 2004
- 2 Average Oil Volume Extracted Daily by Month
- 3 Average Daily Oil and Water Volumes by Month
- 4 Average Daily Oil Volume vs. Average Water/Oil Volume Ratio by Month
- 5 Average Oil Thickness vs. Average Piezometric Groundwater Elevation
- 6 Estimated Oil Thickness Contours May 2000
- 7 Estimated Oil Thickness Contours May 2004

#### REFERENCES

#### **APPENDICES**

- A Total Petroleum Hydrocarbons Fingerprint Chromatograms
- B LNAPL Volume Calculations Backup Information

#### 1.0 INTRODUCTION

This memorandum presents the results of our evaluation of the progress of the Non-Time-Critical Removal Action (NTCRA) at the Beede Waste Oil Site through September 2004. The evaluation looked at trends in oil and water extraction by the Vacuum Enhanced Extraction (VEE) system, oil thickness measurements in system extraction wells from system start-up in February 2000 through September 2004, and the evaluations conducted in recent months to develop a better understanding of the oil plumes and oil volume remaining at the site.

This evaluation was performed by Tetra Tech NUS (TtNUS) at the request of the U.S. Environmental Protection Agency (EPA) under Contract No. 68-W6-0045, Work Assignment No. 105-NARV-011T.

#### 2.0 NTCRA WASTE EXTRACTION EVALUATION

The VEE system commenced operation on February 21, 2000 and continues to operate. Through September 30, 2004, approximately 85,000 gallons of LNAPL and 304,000 gallons of water have been extracted and separated by the VEE system and transported off site for treatment/disposal. The overall ratio of water to oil extracted is approximately 3.6 to 1. Several charts are presented and described below to illustrate trends in waste extraction.

<u>Figure 1</u> shows the cumulative oil and water volumes extracted by the system from February 2000 through September 2004. It appears that the rate of oil recovery was highest during the first several months of operation and has gradually decreased over time. The rate of water recovery was also highest during the initial months of operation. It has decreased from initial rates, but has remained relatively consistent since early 2001.

<u>Figure 2</u> shows the average daily volume of oil extracted each month. The average volumes have fluctuated from month to month. The volumes appear to show a seasonal variation, with the lowest daily volumes typically occurring in the spring, then increasing gradually to a peak in the late fall, and then declining through winter to a spring low. The seasonal variations were less apparent during the first several months of operation, when extraction volumes were consistently high. Comparing average daily extraction volumes

over time, a general decreasing trend is evident, with the exception of a period from fall 2001 through spring 2002. The average extraction volumes observed during this period were higher than during the corresponding months in the previous year. This apparent increase is primarily due to more frequent overnight operation (the overnight volume is included in the volume for the day) and additional rest/recovery days during this period, which both increased the daily extraction volumes. Overnight operation was most frequent during the Fall 2001 to Spring 2002 period due to conditions in the plume, which allowed for relatively efficient operation with minimal system adjustments.

<u>Figure 3</u> shows the average daily volumes of oil and water extracted each month. Trends in oil extraction are discussed above. Unlike oil extraction volumes, water extraction volumes don't exhibit clear seasonal variations. Extraction volumes, in general, appear to have decreased over time, with decreasing oil extraction volumes, but occasional periods of higher water volumes also occur.

<u>Figure 4</u> shows the average water to oil extraction ratios versus the average daily volumes of oil extracted each month. This figure shows an increase in the water/oil ratios over time. In the year from October 2003 through September 2004 the overall water/oil ratio was 5.8.

It appears that the rate of oil recovery has slowed in recent months while the rate of water extraction has remained similar to earlier periods, thereby increasing the ratio of water to oil extracted. This is likely caused by the decrease in oil thickness in the plumes resulting from extraction of approximately 85,000 gallons of oil. As the oil thickness in the plumes and extraction wells decreases it becomes more difficult to extract the oil from the water surface without extracting more water. As the oil thickness has decreased, system operation has required more frequent well/drop-tube adjustments to optimize system operation, extracting as much oil and as little water as possible. The drop in oil extraction rates and rise in water/oil ratios has occurred despite more intensive monitoring and adjustment. However, changes in operation schedule and staffing in recent months appear to have helped increase extraction efficiency, as demonstrated by the lower water/oil ratios observed from June through September 2004.

#### 3.0 OIL THICKNESS EVALUATION

Changes in oil thickness in the VEE system extraction wells were evaluated as an indicator of NTCRA progress. It is generally accepted that the measured oil thickness in a well does not correlate exactly to the thickness in the aquifer formation. Factors that may contribute to the disparity include differences in capillary properties in the formation, the filter pack surrounding the well and the well itself, and fluctuations in the water table. Despite these factors, the measured thicknesses can be used to draw some conclusions about NTCRA progress and status.

Evaluation of site data indicates that the measured oil thicknesses in system extraction wells vary as the groundwater rises and falls. In general, the measured oil thickness in the wells is greatest when the potentiometric groundwater elevations are the lowest and visa versa (see Figure 5). This is consistent w/ conceptual model of LNAPL behavior in the subsurface as described in literature (API, 1999). Because of this relationship between measured oil thickness and groundwater elevation, when evaluating changes in oil thickness it is necessary to compare time periods that have similar groundwater elevations. Four time periods (April-May 2000, 2001, 2003, 2004) representing the highest observed groundwater elevations were selected for evaluation. It is assumed that the oil thickness measured at these times may represent the lowest exaggeration and best correlation between the measured oil thickness in wells and the actual mobile oil thickness in the subsurface. Comparing the average oil thicknesses for these periods on Figure 5, there appears to be an overall trend of decreasing oil thickness at the site from April-May 2000 to May 2004.

During each monitoring event shown on Figure 5, all 143 VEE system extraction wells were monitored with an electronic oil/water interface probe to determine the groundwater elevation and oil thickness. For the monitoring periods compared, the number of wells in nearly every oil thickness bracket has decreased over time, illustrating an overall decrease in oil thickness at the site. Only the number of wells with oil less than 0.25 feet thick has increased significantly from April-May 2000. This thickness interval now constitutes the majority of wells. The relatively consistent number of wells with oil present (greater than 0 ft) indicates that the overall areal extent of the plumes has probably not changed significantly.

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Oil Thickness	Number of Wells With Stated Oil Thickness						
	Apr-May-00	May-01	May-03	May 2004			
5 ft. to 6 ft.	1	0	0	0			
4 ft. to 5 ft.	1	0	0	0			
3 ft. to 4 ft.	3	2	1	0			
2 ft to 3 ft.	6	2	1	2			
1.5 ft. to 2 ft.	5	3	4	0			
1 ft. to 1.5 ft.	9	6	2	2			
0.5 ft. to 1 ft.	24	17	14	11			
0.25 ft. to 0.5 ft.	17	16	19	10			
>0 ft to 0.25 ft	27	59	53	76			
Total > 0 ft	93	105	94	101			

The oil thickness monitoring data were used to prepare estimated oil thickness contour figures for April-May 2000 and May 2004 monitoring periods (see Figures 6 and 7). Comparison of the figures shows that the thickness of the oil plumes has decreased over time, but the areal extent of the plumes doesn't appear to have changed significantly. The decrease in oil thickness is clearly illustrated by the decrease in the size of areas with oil thickness greater than 0.5 feet. Changes in overall plume size are more difficult to assess because several wells show no measurable oil during some periods and then have a measurable thickness in some subsequent periods. The contours have been drawn to show these wells and the surrounding areas as having no oil when no measurable oil was observed; however, the presence of oil in these areas during intervening periods indicates that the plume is likely continuous in these areas, but is very thin (a sheen too thin to measure) or is immobilized in the soil pores during some monitoring periods. The plumes do not appear to be actively migrating. The overall shapes of the plumes have remained relatively consistent over time.

#### 4.0 OIL VOLUME EVALUATION

Estimating the volume of mobile or recoverable oil present in the subsurface at the Beede Waste Oil site is complicated by many factors including those inherent with any LNAPL system, such as the seasonal fluctuation of oil thickness in monitoring wells and the lack of correlation between measured and actual oil thickness in the subsurface. Evaluating the LNAPL system at the Beede site is further complicated by the heterogeneous composition and characteristics of oils across the site, the presence of emulsion in some wells, the presence of

the oil in at least four distinct geologic units, and measurement difficulties for most of the oils present. TtNUS performed two types of evaluations to develop a better understanding of the oil remaining in the subsurface at the site. These are described below.

#### 4.1 Field Evaluations of LNAPL Thickness and Characteristics

Three types of field evaluations were performed by TtNUS to assist in better understanding the nature and extent of LNAPL remaining at the site. This section describes the evaluations performed.

#### Oil and Emulsion Thickness Measurement Evaluation

Obtaining an accurate measurement of the LNAPL thickness in wells at the site is difficult because of the viscosity of the oil and presence of emulsion in some wells. When using a standard electronic interface probe, the viscous oil coats the probe and makes it difficult to detect the oil/water interface; the presence of emulsion beneath the oil makes it difficult to clearly identify the bottom of the oil or the top of the water because the emulsion registers on the probe as a fast beeping tone between those of oil and water (the frequency of the beep can vary to sound similar to an oil or water tone).

To address the measurement difficulty, TtNUS used a custom-designed bailer to collect relatively undisturbed samples of the entire LNAPL column in several monitoring wells. The content of the bailer was observed immediately upon collection and after settling to identify the presence of distinct layers. The thickness of the fluids in the bailers were measured and compared with thickness measurements taken using an LNAPL interface probe to determine the accuracy of the well measurements.

The following conclusions were drawn from the bailer samples and measurements:

 A distinct emulsion layer was identified below the oil layer in several wells. The emulsion layer was generally a distinctly lighter colored layer of a different consistency than the oil.

- In some wells, the LNAPL column consisted of 3 or more different layers (multiple oil and/or emulsion layers).
- The interface probe appears to accurately detect the presence of emulsion in most cases, but does not seem to provide accurate measurements of emulsion thickness.
- Oil thickness measurements taken with the probe generally correlated well with the thickness in the bailer, but emulsion thickness measurements did not correlate well.

#### Waste Characterization

Oil and emulsion samples from five wells (EW-23, EW-34, EW-94, EW-109, and EW-110 – see Figures 6 and 7) were sent to an off-site laboratory for chemical and physical characterization to determine the content and characteristics of the oil and emulsion and to determine the relationship between the oil and the emulsion. The samples were analyzed for VOCs, PCBs, TPH/petroleum hydrocarbon fingerprinting, density, and viscosity. In addition, the emulsion samples were physically separated to determine percent oil, water, and sediment. The analytical results for the oil and emulsion are presented on Tables 1 and 2. TPH fingerprint chromatograms for the oil and emulsion samples and diesel fuel and motor oil standards are presented in Appendix A. The following conclusions were drawn from the waste analyses.

- The oil and emulsion samples from all 5 wells have TPH fingerprint patterns typical of a mix of No. 2 diesel fuel and motor oil, but the mixtures vary across the site. The two samples from the lagoon plume appear to have a greater fraction of motor oil, whereas the samples from the UST plume appear to have a greater fraction of diesel fuel. None of the samples have identical fingerprints.
- The fingerprint patterns from the oil and emulsion samples from the same location were similar.

- The chemical constituents of the NAPLs are fairly similar across the site, but occur in varying concentrations. The resulting NAPLs exhibit very different physical properties.
- The emulsion samples typically have chemical constituents similar to the oil samples
  from the same wells, but sometimes in markedly different concentrations. Most notable
  was that the PCB concentrations in all emulsion samples were nearly double the PCB
  concentrations in the oil sample from the same well.
- The oil densities were similar (0.8745 to 0.8863 g/ml); the emulsion densities showed greater variation (0.888 to 0.9646 g/ml). The emulsion samples were heavier than the corresponding oil samples.
- Oil viscosities ranged from 53.93 to 136.3 CTS. Emulsion viscosities ranged from 148.3 to 2196 CTS. The emulsion samples were more viscous than the corresponding oil samples.
- The emulsion appears to be derived from the oil in the same area. However, it is not clear whether the emulsion is a settled component of the original waste oil mixture (possibly a heavier fraction with more suspended solids), whether it is created in the subsurface as a result of naturally occurring subsurface conditions such as biological activity, or whether it is created in the wells (and possibly the surrounding area) as a result of the vacuum extraction process.
- The extent of the emulsion presence in the subsurface is uncertain because its presence has only been noted sporadically at most wells where it has been detected. It appears to be present most consistently in the areas north of soil stockpile 5A (wells 99 101, 109, 110, 115) and in/near surface water retention pit 2 (SWRP 2) (wells 124, 131, 137, 138). However, even in these wells it has not been detected during every monitoring period.
- The properties of the emulsion, particularly the high viscosity, may further complicate LNAPL extraction if it is present on a large scale because it will likely be less mobile and more difficult to remove from the soil pore spaces.

#### Monitoring Well and Subsurface Oil Thickness Relationship

TtNUS conducted product recovery tests in several wells to determine whether a relationship could be established between the observed thickness in the wells and the actual thickness in the aquifer. The tests were conducted using a procedure adapted from methods presented by Hughes, et al. (1988), and Aral and Liao (2000). These methods involve evacuating the LNAPL from a well and monitoring and plotting its recovery to identify the inflection point, which corresponds to the LNAPL entry point – or bottom of the mobile LNAPL layer in the formation. The LNAPL thickness measured at the inflection point is used to estimate the actual LNAPL thickness in the aquifer. In theory, the LNAPL recovery rate will remain constant until air/LNAPL interface in the well rises to the LNAPL entry point, and will then steadily decrease as the LNAPL surface in the well rises above the entry point. The plot of the LNAPL thickness during recovery is evaluated to identify the inflection point.

Product recovery tests were attempted in several wells (EW-22, EW-26, EW-29, EW-86, EW-116, and EW-110). The test results at all wells were determined to be inconclusive because either the inflection point could not be identified or the recharge curve did not fit the profile required to estimate product thickness using this method (initial constant recharge rate followed by a decreasing recharge rate). The principal problems that impeded successful tests were: monitoring difficulties due to the viscous oil and emulsion, slow recovery, and lack of overnight monitoring of recovery. Monitoring difficulties in combination with slow recovery were the most significant problem. In some cases, due to slow recovery and viscous oil, the process of measuring the oil thickness removed much or all of the product that had recovered since the last measurement.

### 4.2 <u>Estimation of LNAPL Volume Based on API/Lenhard-Parker Equations</u>

TtNUS attempted to estimate the volume of mobile LNAPL remaining at the site using equations and methods provided in the following peer-reviewed publications: Free-Product Recovery of Petroleum Hydrocarbon Liquids, API, 1999; and Estimation of Free Hydrocarbon Volume from Liquid Levels in Monitoring Wells, Lenhard and Parker, 1990. These methods are based on the premise that LNAPL is part of a multi-phase saturation system with unique responses based on both specific soil types and LNAPL properties. In theory, in the

subsurface, each LNAPL will have a distinct saturation profile based on the LNAPL type and subsurface lithology. Accurate estimations of LNAPL volume in the subsurface are dependent upon understanding the site-specific capillary pressure response curve for each plume and distinct lithology. In other words, a distinct capillary pressure response curve should be developed for each area of the plume where the LNAPL characteristics and/or lithology changes.

For many sites, the LNAPL type is one consistent type, and may only occur over one or two distinct lithologies. However, at the Beede Waste Oil site, several LNAPLs occur simultaneously over at least four distinct lithologies (sand, fine sand, gravelly sand, and fill). Though the variance of LNAPL type itself may not significantly affect the capillary pressure curve, it is important to consider many site-specific capillary pressure curves in representative portions of the plumes in order to ensure that an accurate calculation is performed. At a bare minimum, one capillary pressure curve should be developed for each lithology.

Site-specific data is always recommended. However, it is typically not available, as in this case. In absence of site-specific data, input parameters were selected from literature values based on site-specific soil types, conductivity parameters, and LNAPL properties. Since sand is the dominant soil type, an average sand lithology was selected. Because sand has a wide range of potential properties, the resulting range of potential literature values for the capillary fit parameters was quite large, usually encompassing the full spectrum of legitimate values. Average values were selected as representative inputs (see attachment for selected values).

Calculations were made with the TtNUS LNAPL volume estimation routine that explicitly solves for the unit volume in soil and then uses the affected area to determine the total volume. Two test cases were also run, one with API's volume estimation routine (using same input) as a check and one example with modified input parameters. All three sets of calculations resulted in an obvious gross under-estimation of the total volume of oil present at the site. The general conclusion from this evaluation is that this methodology, although applicable to the problem at the site, could only be employed effectively here if a large amount of site-specific data were available. Selecting alternative input values from published sources would not provide a greater degree of certainty because the range of capillary fit parameters for sands is very large, the range of LNAPL characteristics varies widely across the site, and the possible matrix

of LNAPL/ lithology combinations is too large to reasonably derive average conditions for the site.

Collecting site-specific data to develop more representative capillary pressure curves could improve the accuracy of the volume calculations. However, since the number of lithologies and wide range of LNAPL present (including various types of oil and emulsion) create numerous possible lithology/LNAPL combinations, a large amount of site-specific data (i.e. specialized analysis of LNAPL samples and undisturbed cores of the LNAPL saturated soils from many locations within the plumes) would be required to provide a reasonable degree of certainty in the accuracy of the calculations. To provide the highest degree of certainty, all possible combinations of LNAPL and lithology would have to be sampled. This scale of investigation is not recommended because it is unlikely to provide benefits commensurate with its cost.

#### 4.3 <u>LNAPL Volume Evaluation Summary</u>

In conclusion, field evaluations and laboratory characterization of the LNAPL at the site confirms that the LNAPL plumes at the site are comprised of oils and emulsions with widely varying chemical and physical properties. The physical properties of the LNAPLs make it difficult to accurately measure their thickness in site monitoring wells. Additionally, the varying properties cause the LNAPLs to have different behaviors in the subsurface. The presence of the LNAPL in several different geologic units further complicates the situation, as LNAPL will behave differently in different lithologies. As a result of all of these factors, the LNAPL saturation profiles of each LNAPL in each of the geologic unit at the site will differ.

Because of the complexity of the LNAPL plumes and lithology at the Beede Waste Oil site and the inherent difficulties in relating widely varying well thickness measurements to actual LNAPL volume in the subsurface, it is not possible, with the available data, to develop LNAPL volume estimates for the site with a high degree of certainty. However, based on the significant LNAPL thickness still routinely present in many wells and the continuing ability of the VEE system to extract an average of nearly 50 gallons of LNAPL daily, it appears that a significant volume of recoverable LNAPL remains at the site.

TABLES

## TABLE 1 OIL AND EMULSION ANALYTICAL RESULTS - DETECTED COMPOUNDS ONLY TECHNICAL MEMORANDUM BEEDE WASTE OIL SITE PLAISTOW, NEW HAMPSHIRE

	BWO-OIL-	BWO-EMUL-	BWO-OIL-	BWO-EMUL-	BWO-OIL-	BWO-OIL-	BWO-EMUL-	BWO-OIL-	BWO-EMUL-
ICamamia Mumahar		EW23	EW34	EW34	EW94	EW109	EW109	EW110	EW110
1		Fmr. Lagoon	Fmr. Lagoon	Fmr. Lagoon	UST	UST	UST	UST	UST
Date Sampled	•	7/27/2004	7/26/2004	7/26/2004	7/26/2004	7/27/2004	7/26/2004	7/26/2004	7/26/2004
ļ ·	None	None	None	None	None	None	None	None	None
QC Identifier	None	110116	110110	TTO IIC		T			
Volatile Organic Analysis (UG/KG)	1122		07000	0500	890 J	2500 U	2500 U	2500 U	2500 U
1,1,1-Trichloroethane	11000	7300	37000	9500	1700 J	2500 U	2500 U	2500 U	2500 U
1,1,2-Trichloro-1,2,2-trifluoroethane	2200 J	1400 J	2200 J	500 J	1/00 3	2500 0	3300	2300 0	2500 U
1,1,2-Trichloroethane		2500 U	200	2500 U	1500 J	2500 U	2500 U	2500 U	2500 U
1,1-Dichloroethane	440 J	290 J	360 J	2500 U	2500 U	2500 U	2500 U	2500 U	2500 U
1,1-Dichloroethene	1800 J	780 J	5400	1300 J	1500 J	2500 U	820 J	1300 J	2500 U
1,2,4-Trichlorobenzene	430 J	260 J	440 J	2500 U	17000 J	2500 U	2100 J	9400	2500 U
1,2-Dichlorobenzene	12000	6600	17000	3900	1/000	2500 0	2500 U	3400	2500 U
1,2-Dichloroethane		2500 U	4005	330 J	1700 J	2500 U	520 J	1100 J	2500 U
1,3-Dichlorobenzene	1200 J	690 J	1300 J	330 J	5600	2500 U	1500 J	3000	2500 U
1,4-Dichlorobenzene	2900	1800 J	3300	850 J	1900 J	2500 U	1100 J	1700 J	2500 U
2-Butanone	2100 J	1500 J	2500 U	2100 J	2500 U	2500 U	1100 3	2500 U	2300 0
2-Hexanone	12000	2500 11	2500 U	2500 U	2500 U	2500 U	260 J	650 J	2500 U
Acetone	2500 U	2500 U	2500 U	2500 U 5800	1200 J	2500 U	2500 U	2500 U	2500 U
Benzene	520 J	340_J	19000	5600	260 J	2500 U	2300 0	2500 U	2000 0
Chloroethane	2500 U	4000	2500 U 38000	13000	2500 U				
cis-1,2-Dichloroethene	6100	4200	2500 U	13000	2500 U	2500 U	2500 0	1900 J	- 2000
Cyclohexane	2500 U	000	2500 0	2500 U		2300 0	2500 U		2500 U
Dibromochloromethane	05000	860 J	110000 *	30000	36000	2700	1500 J	11000	9800
Ethylbenzene	35000	22000	19000	4800	10000	1500 J	680 J	3800	2100 J
Isopropylbenzene	8000	4300 6700	39000	9900	64000	9700	4000	20000	4500
Methylcyclohexane	12000 3500	2100 J	11000	3000	5200	2500 U	550 J	2200	2500 U
Styrene	2100 J	1300 J	4400	1200 J	1200 J	790 J	2500 U	590	350 J
Tetrachloroethene	18000	11000	280000 *	54000 *	48000	2100	1100 J	5400	7100
Toluene	150000 *	120000	740000	140000	280000	53000	28000	110000	79000
Total Xylenes	2500 U	2500 U	14000	4200	2500 U				2500 U
Trichloroethene	2500 0	2300 0	14000	7200	2000 0	2000 0			
PCB Analysis (UG/KG) Aroclor-1242	20000	43000	23000	42000	21000	28000	68000	34000	65000
Aroclor-1242 Aroclor-1260	9000	17000	7200	13000	22000	28000	66000	25000	46000
	3000	17000	7200	10000	2200	1 20000	30000		
Extractable Total Petroleum Hydrocarbon									
Analysis (MG/KG)	640000	790000	680000	620000	940000	650000	710000	740000	760000
Total Petroleum Hydrocarbons	040000	7 30000	000000	020000	540500	+	7.5550	7.13330	
Wet Chemistry Analysis	0.8863	0.888	0.8808	0.9646	0.8745	0.8866	0.9415	0.8777	0.9473
Density @25 deg C	136.3	148.3	94.11	2196	53.93	118.4	626.7	70.96	667.1
Kinematic Viscosity @25 deg C	130.3	140.3	1 94.11	2130	1 33.33	110.4	1 020.7	70.00	

U - Not detected; UJ - Detection limit approximate; J - Quantitation approximate;

R - Rejected; NA - Not Analyzed: \* - From dilution analysis; Blank - not detected in media

## TABLE 2 LNAPL EMULSION COMPOSITION TECHNICAL MEMORANDUM BEEDE WASTE OIL SITE PLAISTOW, NEW HAMPSHIRE

		PERCENT BY VOLUME AFTER SEPARATION*					
EPA ID	WELL ID	OIL	EMULSION	SEDIMENT	WATER		
D13224	EW-23	9.0%	50.7%	35.8%	4.5%		
D13222	EW-34	8.1%	0.0%	87.5%	4.4%		
D13218	EW-109	6.1%	31.7%	37.9%	24.3%		
D13220	EW-110	7.7%	33.4%	28.8%	30.0%		

<sup>\*</sup> Separation by centrifuge (3 minutes @ 3000 rpm + 3 minutes @ 4000 rpm) plus gravity settling.

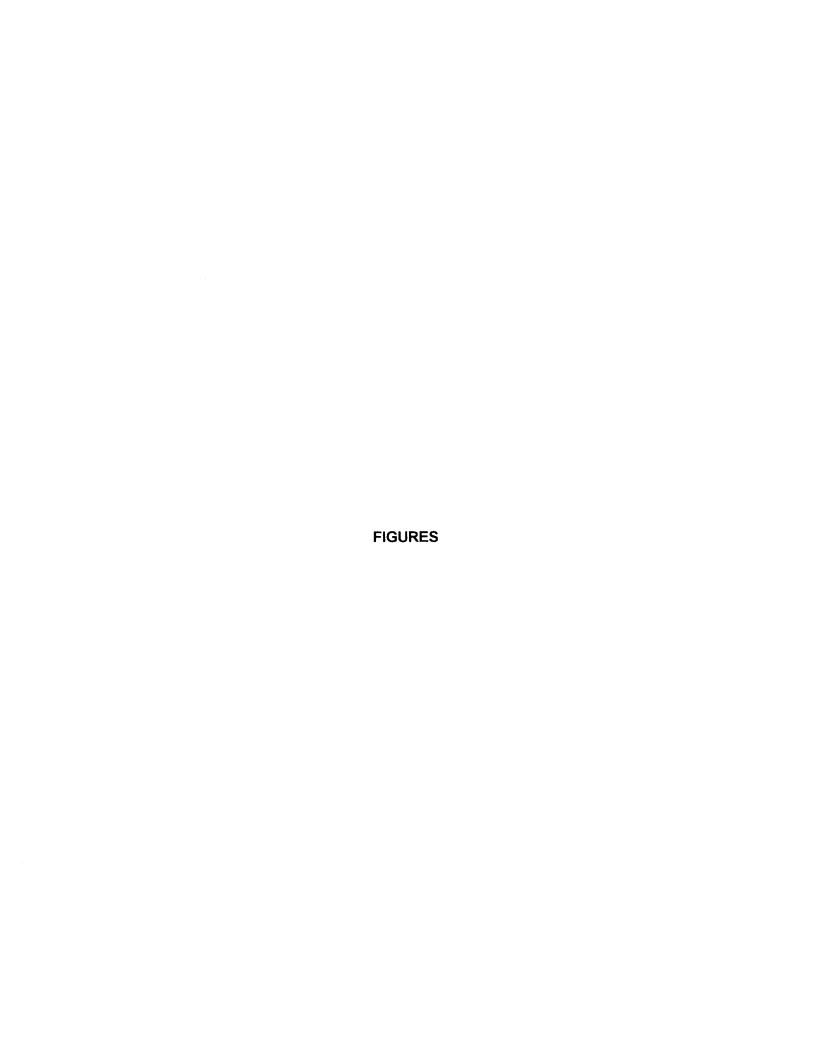


FIGURE 1
CUMULATIVE OIL AND WATER EXTRACTED THROUGH SEPTEMBER 2004
BEEDE WASTE OIL SITE NTCRA

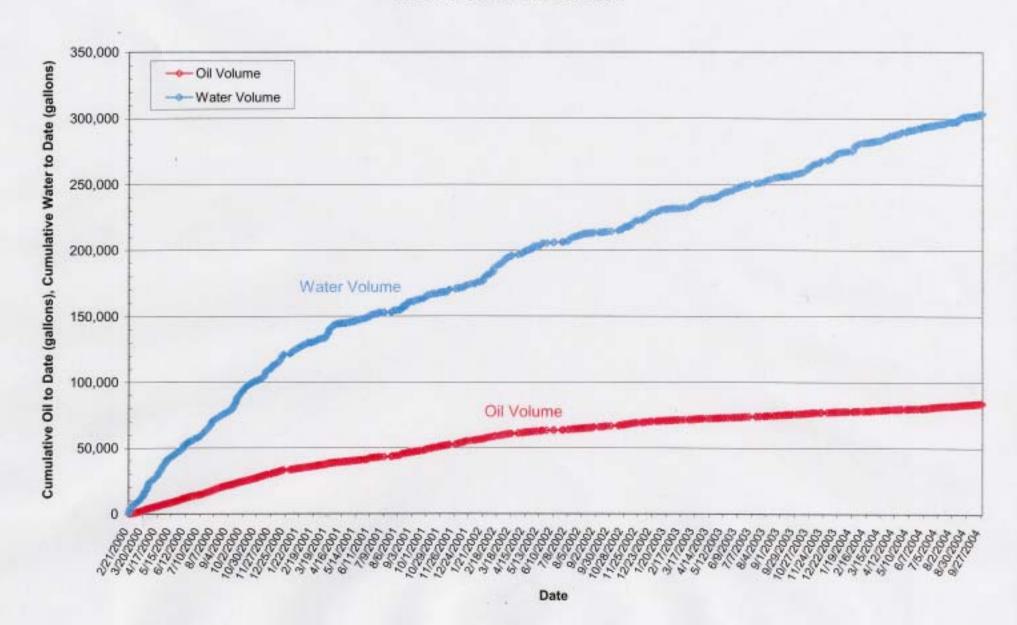


FIGURE 2
AVERAGE OIL VOLUME EXTRACTED DAILY - BY MONTH
BEEDE WASTE OIL SITE NTCRA

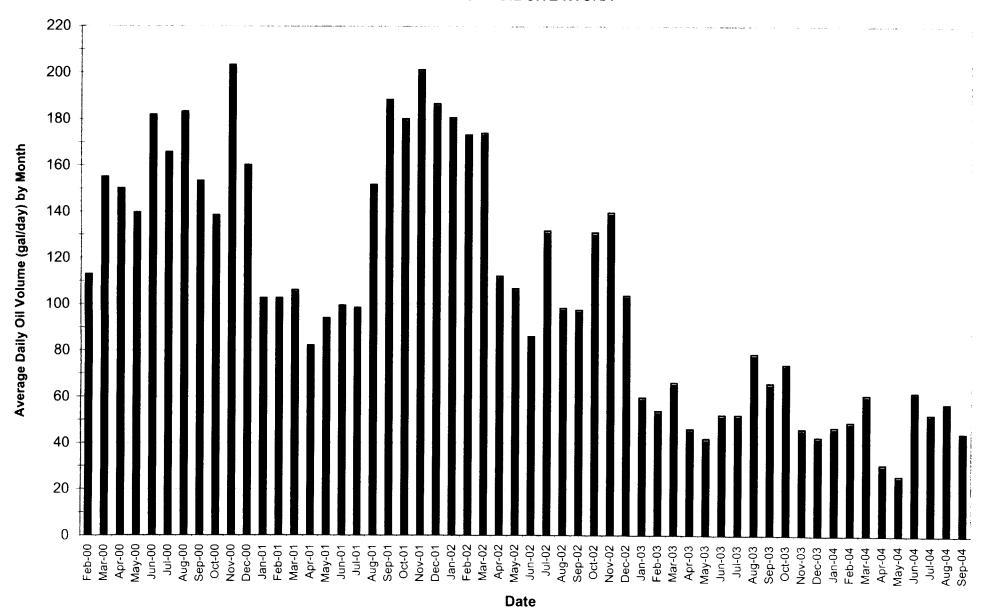


FIGURE 3
AVERAGE DAILY OIL AND WATER VOLUMES BY MONTH
BEEDE WASTE OIL SITE NTCRA

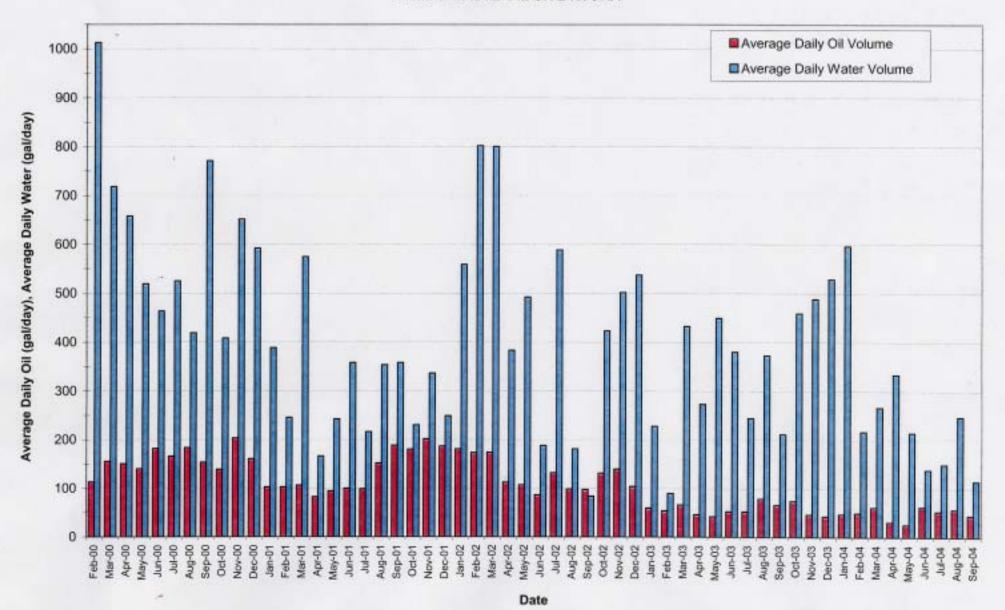
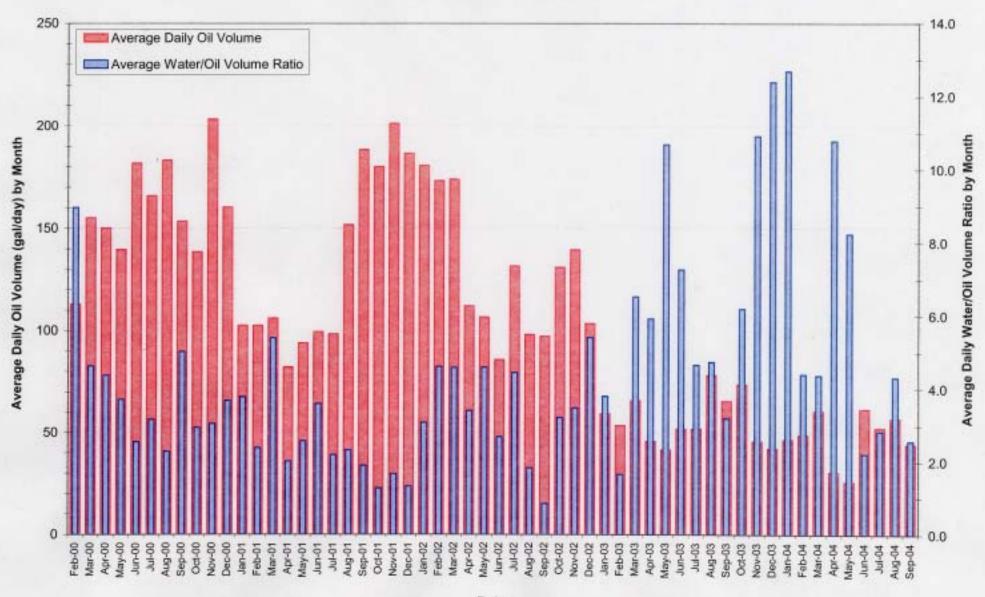
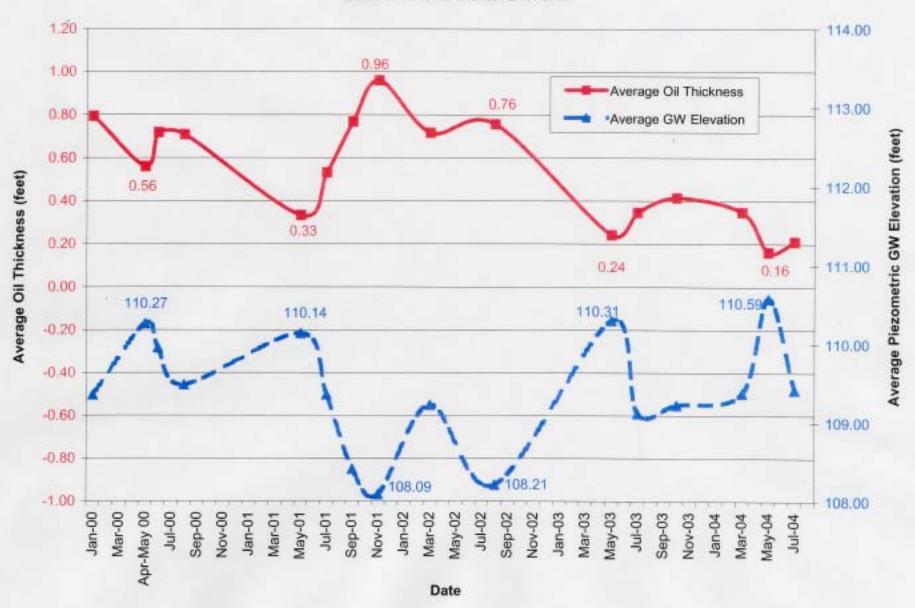


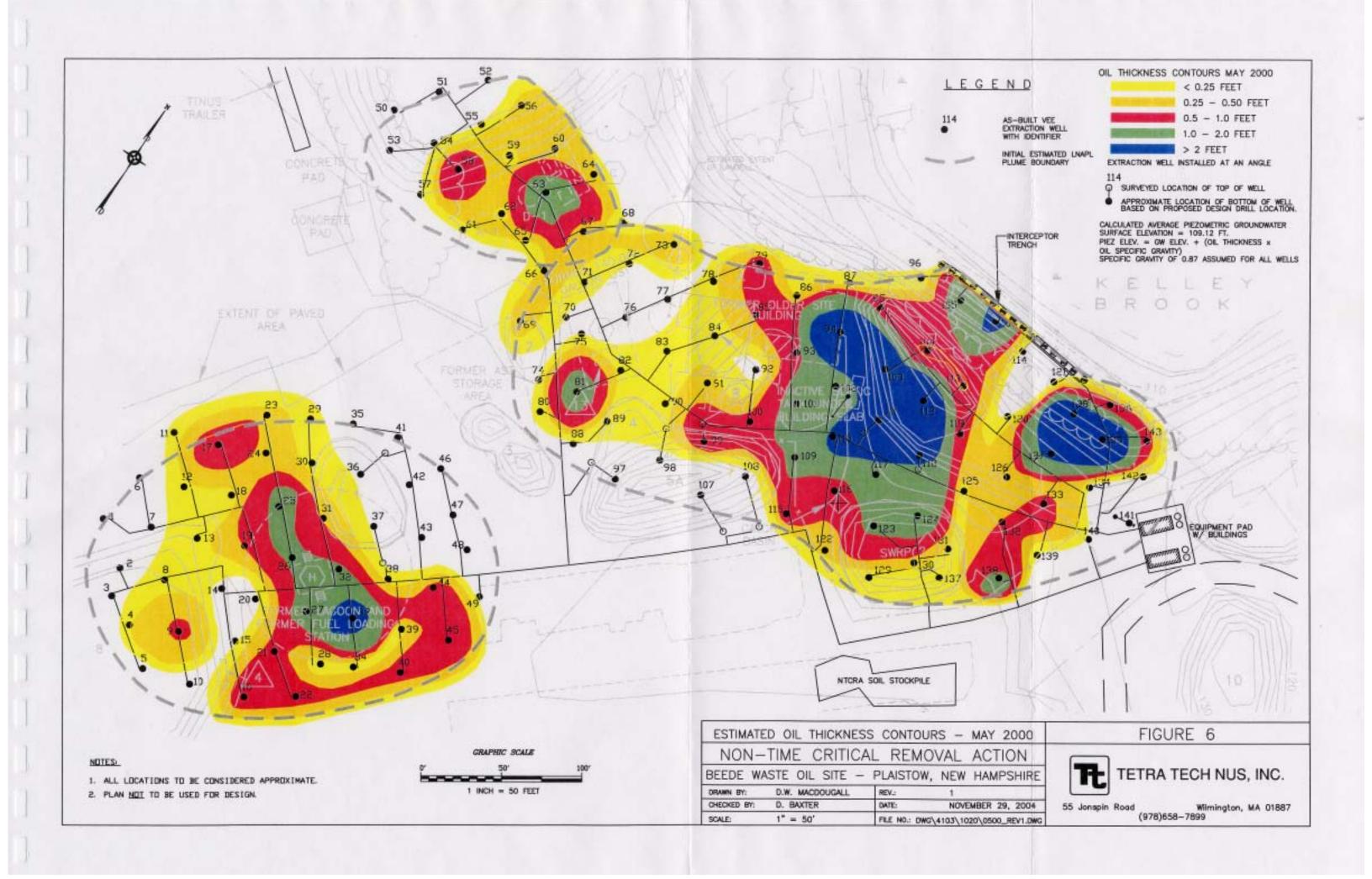
FIGURE 4
AVERAGE DAILY OIL VOLUME VS AVERAGE WATER/OIL VOLUME RATIO - BY MONTH
BEEDE WASTE OIL SITE NTCRA

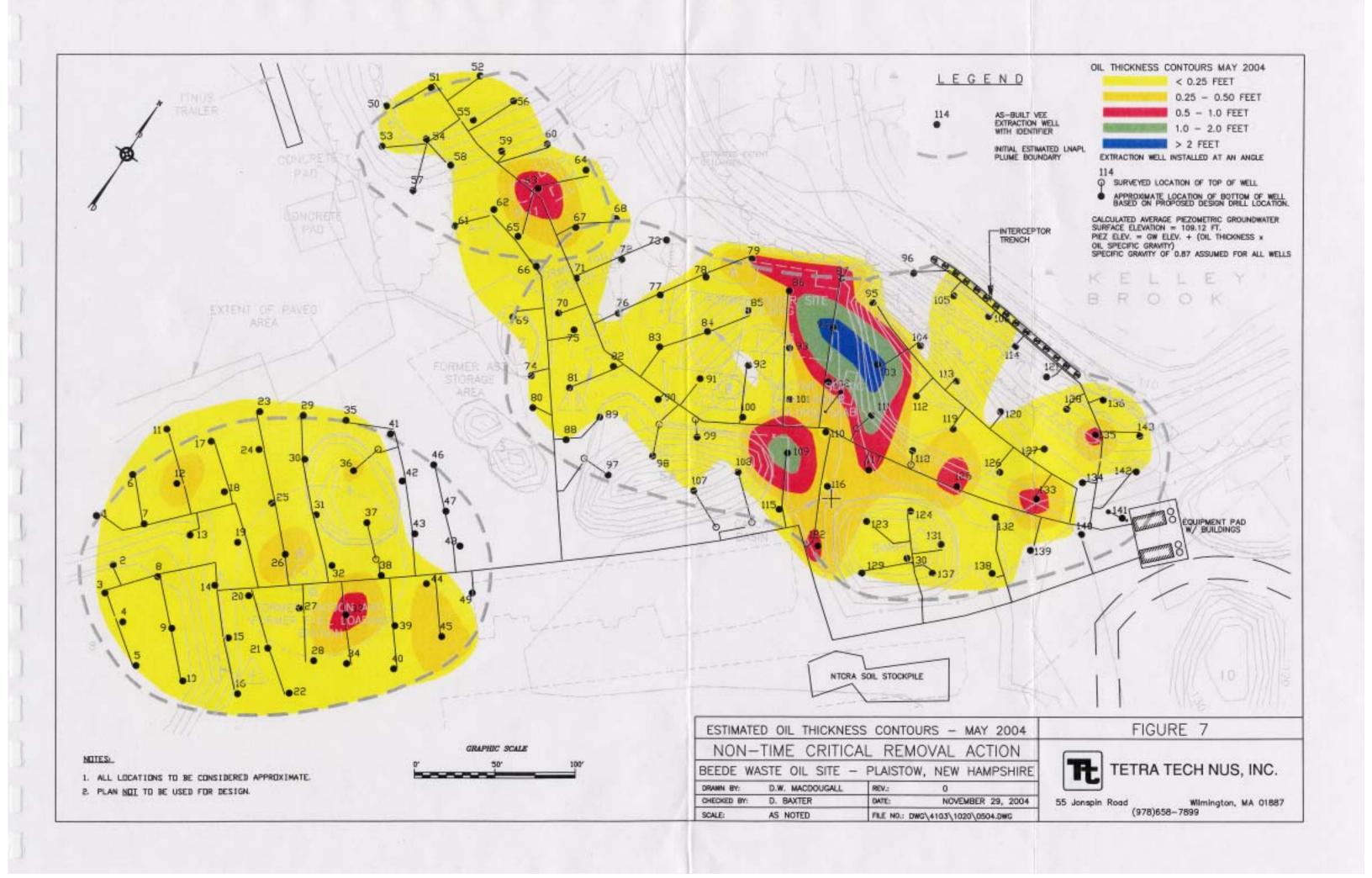


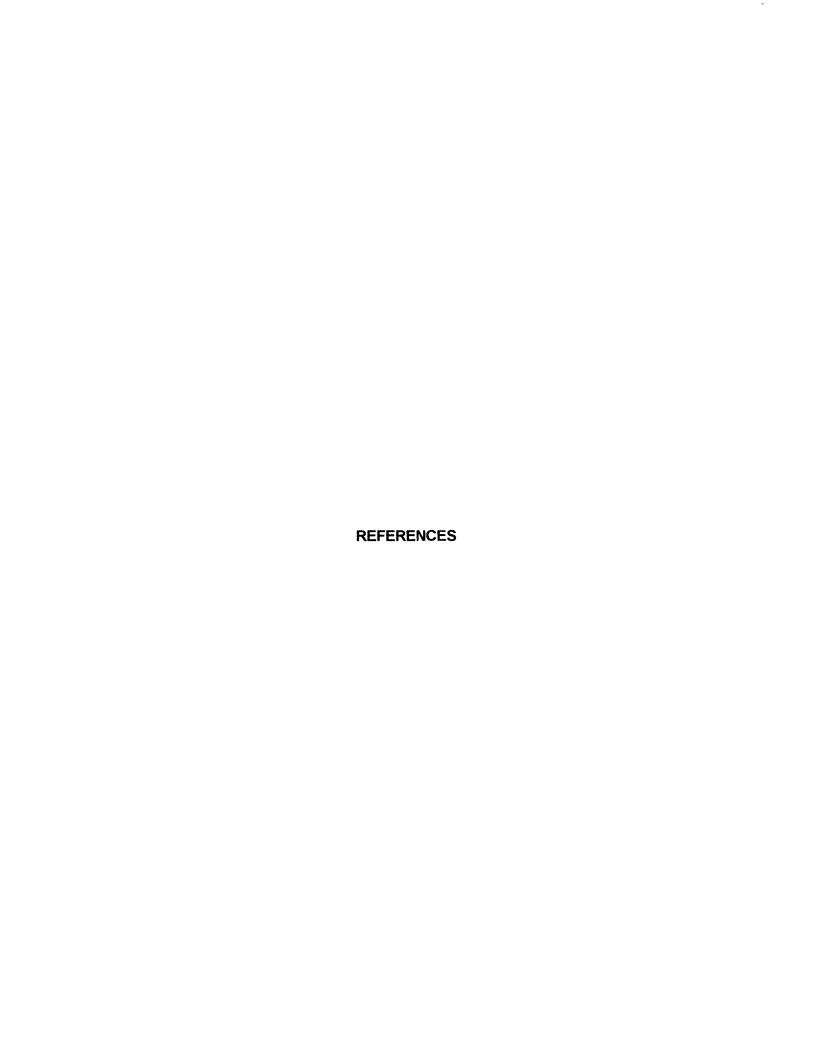
Date

FIGURE 5
AVERAGE OIL THICKNESS VS AVERAGE PIEZOMETRIC GROUNDWATER ELEVATION
BEEDE WASTE OIL SITE NTCRA









#### REFERENCES

American Petroleum Institute,1999. <u>Free-Product Recovery of Petroleum Hydrocarbon</u>
Liquids, June 1999. American Petroleum Institute Publication Number 4682.

American Petroleum Institute, 2003. <u>Models for Design of Free-Product Recovery Systems for Petroleum Hydrocarbon Liquids</u>, August 2003. American Petroleum Institute Publication Number 4729.

Aral, Mustafa M. and Liao, Boshu, 2000. *LNAPL Thickness Interpretation Based on Bail-Down Tests*. Groundwater, Vol. 38, No. 5, September–October, 2000.

Hughes, John P., Clay R. Sullivan, and Ronald E. Zinner, 1992. Two Techniques for Determining the True Hydrocarbon Thickness in an Unconfined Sandy Aquifer. Proceedings of the Conference on Petroleum Hydrocarbons and Organic Chemicals in Groundwater: Prevention, Detection, and Restoration, November 1988.

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#### APPENDIX A

TOTAL PETROLEUM HYDROCARBONS FINGERPRINT CHROMATOGRAMS

Data File : C:\HPCHEM\1\DATA\AUG04\040819\F1D6966.D

Vial: 8

: 8-19-04 15:53:00 PM Acq On

Operator: TT

: C0809-11B X20 Sample

: F1 Inst Multiplr: 1.00

Misc : AUTOINT1.E IntFile

Quant Time: Aug 19 16:32 19104 Quant Results File: ET0304F.RES

Quant Method : C:\HPCHEM\1\QMETHODS\ET0304F.M (Chemstation Integrator)

: TPH-GC, Fuel ID, DRO Title

Last Update : Fri Aug 13 08:50:23 2004

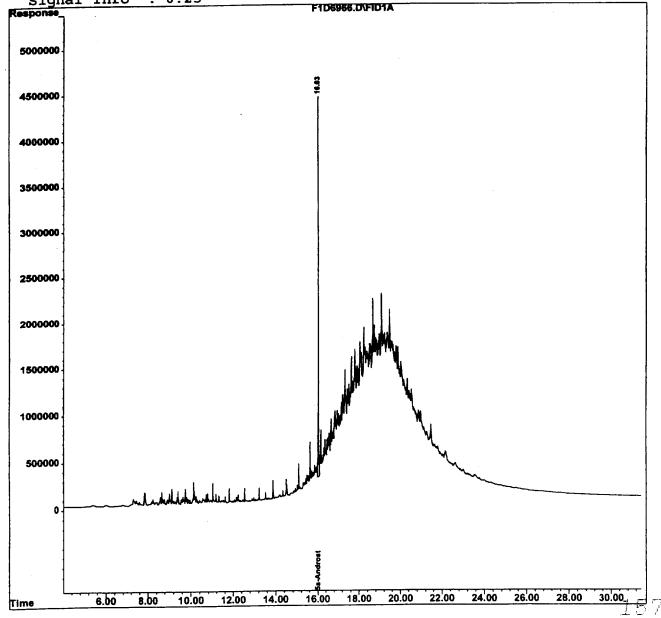
Response via : Multiple Level Calibration

D13223

DataAcq Meth : ETPH-B.M

BWO- OIL- EWZ3

Volume Inj. : 1 Signal Phase : DB-5MS Signal Info : 0.25



Data File : C:\HPCHEM\1\DATA\AUG04\040819\F1D6968.D Vial: 9 Operator: TT : 8-19-04 16:31:07 PM Inst

: C0809-12B X20 : F1 Sample Multiplr: 1.00 Misc

: AUTOINT1.E IntFile

Quant Time: Aug 20 8:44 19104 Quant Results File: ET0304F.RES

Quant Method : C:\HPCHEM\1\QMETHODS\ET0304F.M (Chemstation Integrat

: TPH-GC, Fuel ID, DRO Title

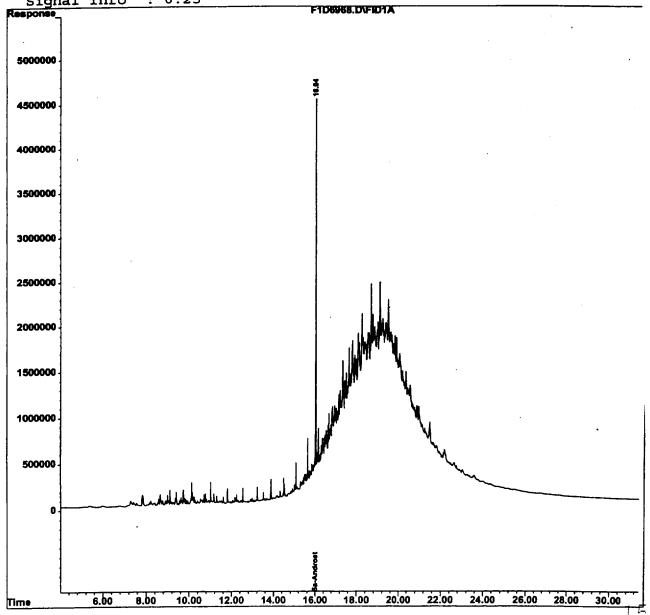
Last Update : Fri Aug 13 08:50:23 2004 Response via : Multiple Level Calibration

D13224

BWO- EMUL - EN DataAcq Meth : ETPH-B.M

Volume Inj. : 1

Signal Phase : DB-5MS Signal Info : 0.25



F1D6968.D ET0304F.M

Fri Aug 20 08:45:04 2004

Data File : C:\HPCHEM\1\DATA\AUG04\040819\F1D6962.D Vial: 6
Acg On : 8-19-04 14:36:25 PM Operator: TI

 Acq On
 : 8-19-04 14:36:25 PM
 Operator: TT

 Sample
 : C0809-09B X20
 Inst : F1

 Misc
 : Multiplr: 1.00

IntFile : AUTOINT1.E

Quant Time: Aug 19 15:32 19104 Quant Results File: ET0304F.RES

Quant Method: C:\HPCHEM\1\QMETHODS\ET0304F.M (Chemstation Integrator)

Title : TPH-GC, Fuel ID, DRO

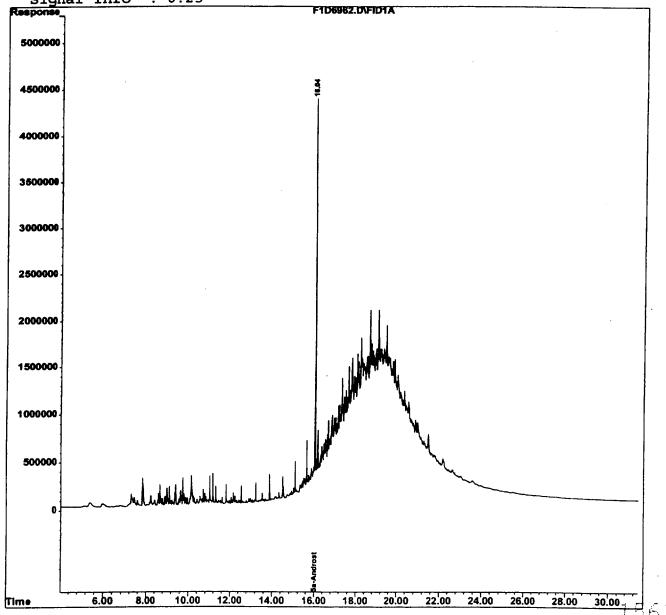
Last Update: Fri Aug 13 08:50:23 2004

Response via: Multiple Level Calibration D13 221

DataAcq Meth: ETPH-B.M BW0-01L-EW34

Volume Inj. : 1

Signal Phase : DB-5MS Signal Info : 0.25



Data File : C:\HPCHEM\1\DATA\AUG04\040819\F1D6964.D Vial: 7 Acq On : 8-19-04 15:14:37 PM Operator: TT Sample : C0809-10B X20 Inst : F1 Multiplr: 1.00 Misc

: AUTOINT1.E IntFile

Quant Time: Aug 19 15:52 19104 Quant Results File: ET0304F.RES

Quant Method : C:\HPCHEM\1\QMETHODS\ET0304F.M (Chemstation Integrat

: TPH-GC, Fuel ID, DRO Title

Last Update : Fri Aug 13 08:50:23 2004

Response via : Multiple Level Calibration

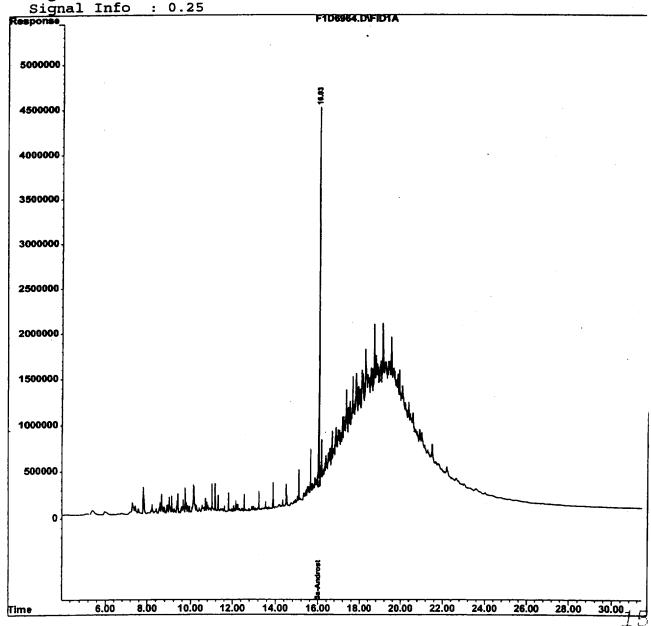
DataAcq Meth : ETPH-B.M

D13222

BWO- EMUL

Volume Inj. : 1

Signal Phase : DB-5MS



F1D6964.D ET0304F.M

Thu Aug 19 15:53:15 2004

Data File : C:\HPCHEM\1\DATA\AUG04\040819\F1D6952.D : 8-19-04 11:25:16 PM

Vial: 1 Operator: TT

Acq On : C0809-04B X20 Sample Misc

Inst : F1 Multiplr: 1.00

IntFile : AUTOINT1.E

Quant Time: Aug 19 14:31 19104 Quant Results File: ET0304F.RES

Quant Method : C:\HPCHEM\1\QMETHODS\ET0304F.M (Chemstation Integrator)

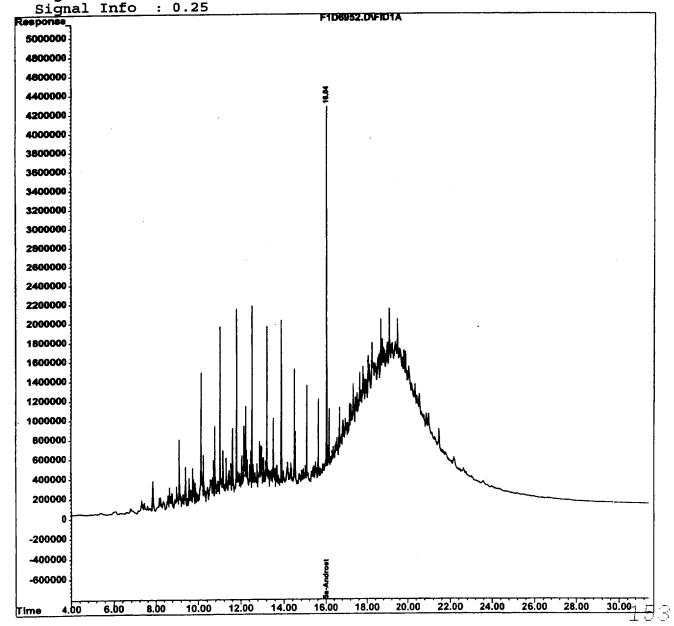
: TPH-GC, Fuel ID, DRO Title

Last Update : Fri Aug 13 08:50:23 2004 Response via : Multiple Level Calibration

DataAcq Meth : ETPH-B.M

D13216 BWO-016-EW94

Volume Inj. : 1 Signal Phase : DB-5MS



Data File : C:\HPCHEM\1\DATA\AUG04\040819\F1D6954.D

Vial: 2 : 8-19-04 12:03:29 PM Operator: TT : C0809-05B X20 Inst : F1

Sample Misc Multiplr: 1.00

: AUTOINT1.E IntFile

Quant Time: Aug 19 14:33 19104 Quant Results File: ET0304F.RES

Ouant Method: C:\HPCHEM\1\QMETHODS\ET0304F.M (Chemstation Integrat

: TPH-GC, Fuel ID, DRO Title

Last Update : Fri Aug 13 08:50:23 2004

Response via : Multiple Level Calibration D13217

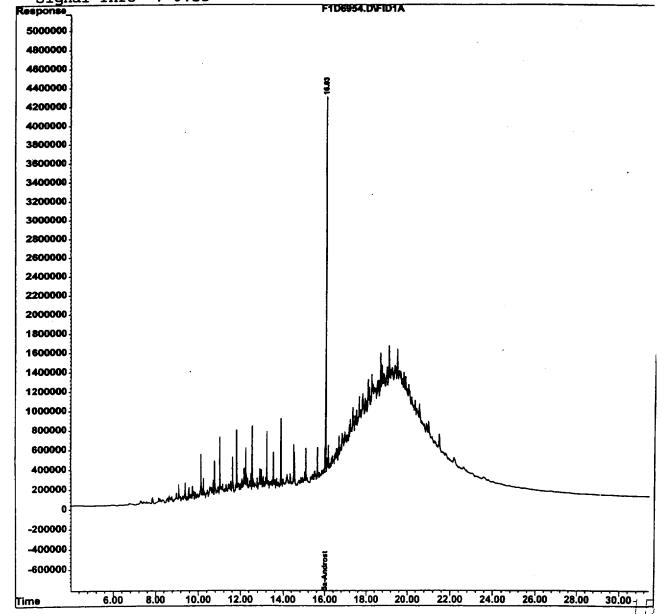
DataAcq Meth : ETPH-B.M

BWO- OIL - EW 199

Volume Inj.

Acq On

Signal Phase : DB-5MS Signal Info : 0.25



F1D6954.D ET0304F.M

Data File : C:\HPCHEM\1\DATA\AUG04\040819\F1D6956.D Vial: 3

Acq On : 8-19-04 12:41:40 PM

Operator: TT Inst : F1

Sample : C0809-06B X20

Multiplr: 1.00

Misc : IntFile : AUTOINT1.E

Quant Time: Aug 19 14:35 19104 Quant Results File: ET0304F.RES

Quant Method : C:\HPCHEM\1\QMETHODS\ET0304F.M (Chemstation Integrator)

Title : TPH-GC, Fuel ID, DRO

Last Update : Fri Aug 13 08:50:23 2004

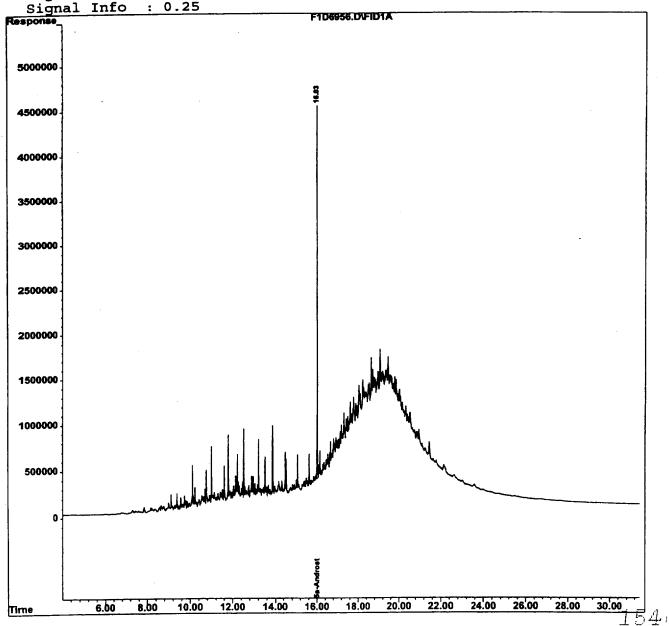
Response via : Multiple Level Calibration

DataAcq Meth : ETPH-B.M

DIBZIB BWO- EMUL - EWIDA

Volume Inj. : 1

Signal Phase : DB-5MS



Data File: C:\HPCHEM\1\DATA\AUG04\040819\F1D6958.D Vial: 4

Acg On : 8-19-04 13:19:53 PM Operator: TT Sample : C0809-07B X20 Inst : F1 Misc Multiplr: 1.00

: AUTOINT1.E IntFile

Quant Time: Aug 19 14:38 19104 Quant Results File: ET0304F.RES

Quant Method: C:\HPCHEM\1\QMETHODS\ET0304F.M (Chemstation Integrat

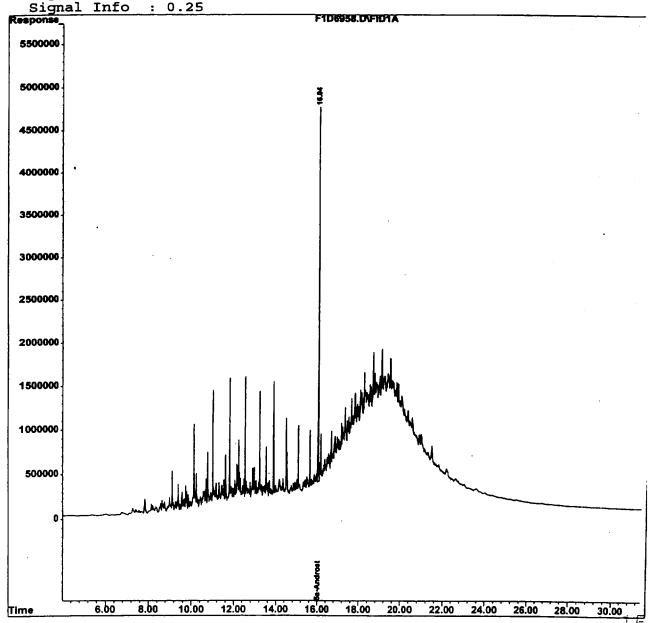
: TPH-GC, Fuel ID, DRO Title

Last Update : Fri Aug 13 08:50:23 2004

Response via : Multiple Level Calibration

BWO-OIL-EWII DataAcq Meth : ETPH-B.M

Volume Inj. : 1 Signal Phase : DB-5MS Signal Info : 0.25



ET0304F.M F1D6958.D

D13219

Data File : C:\HPCHEM\1\DATA\AUG04\040819\F1D6960.D

Vial: 5

Acq On : 8-19-04 13:58:08 PM : C0809-08B X20

Operator: TT Inst : F1

Sample Misc

Multiplr: 1.00

: AUTOINT1.E IntFile

Quant Time: Aug 19 14:40 19104 Quant Results File: ET0304F.RES

Quant Method : C:\HPCHEM\1\QMETHODS\ET0304F.M (Chemstation Integrator)

: TPH-GC, Fuel ID, DRO

Last Update : Fri Aug 13 08:50:23 2004

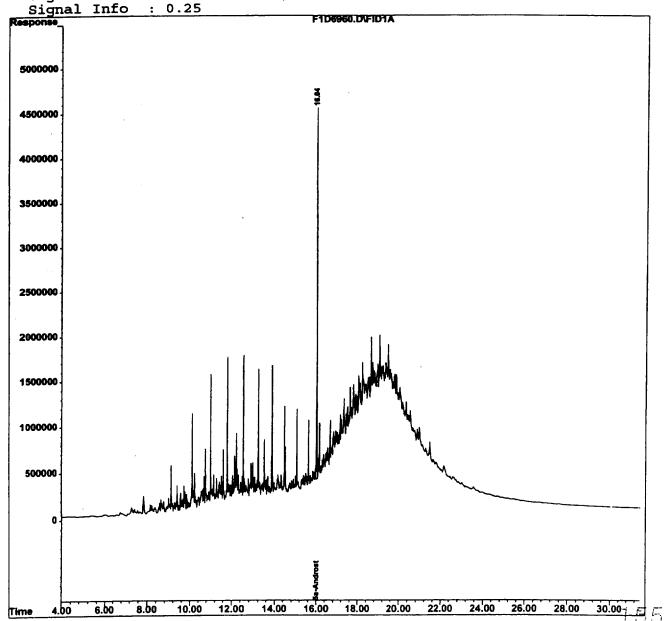
Response via : Multiple Level Calibration

D13220 DataAcq Meth : ETPH-B.M

BWO-ENUL-EWII

Volume Inj. : 1

Signal Phase : DB-5MS



#### Quantitation Report

Data File : C:\HPCHEM\1\DATA\AUG04\040818\F1D6924.D

: 8-18-04 20:54:55 PM

Vial: 2 Operator: TT Inst : F1

Sample

Acq On

: LCS-14098

Inst : F1
Multiplr: 1.00

Misc : IntFile : AUTOINT1.E

Quant Time: Aug 19 10:05 19104 Quant Results File: ET0304F.RES

Quant Method : C:\HPCHEM\1\QMETHODS\ET0304F.M (Chemstation Integrat

Title : TPH-GC, Fuel ID, DRO

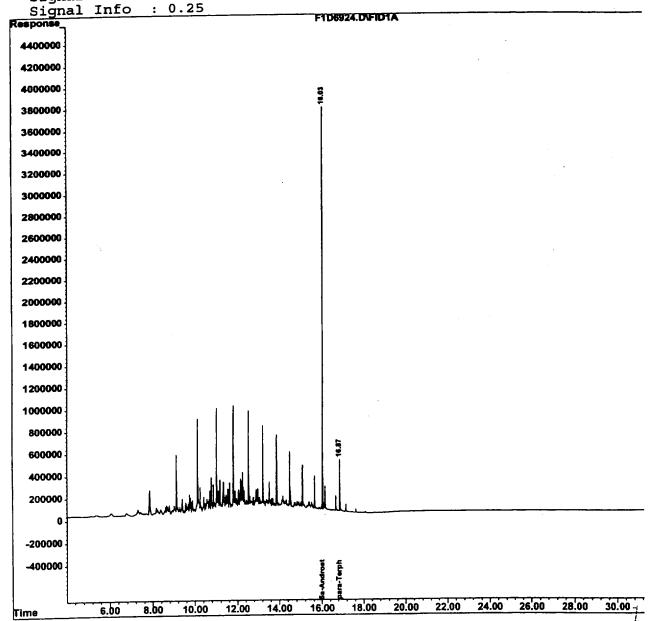
Last Update : Fri Aug 13 08:50:23 2004 Response via : Multiple Level Calibration

DataAcq Meth : ETPH-B.M

Volume Inj. : 1

Signal Phase : DB-5MS

Diesel No Z fuel Standard



File : C:\HPCHEM\1\DATA\AUG04\040819\F1D6974.D

Operator : TT

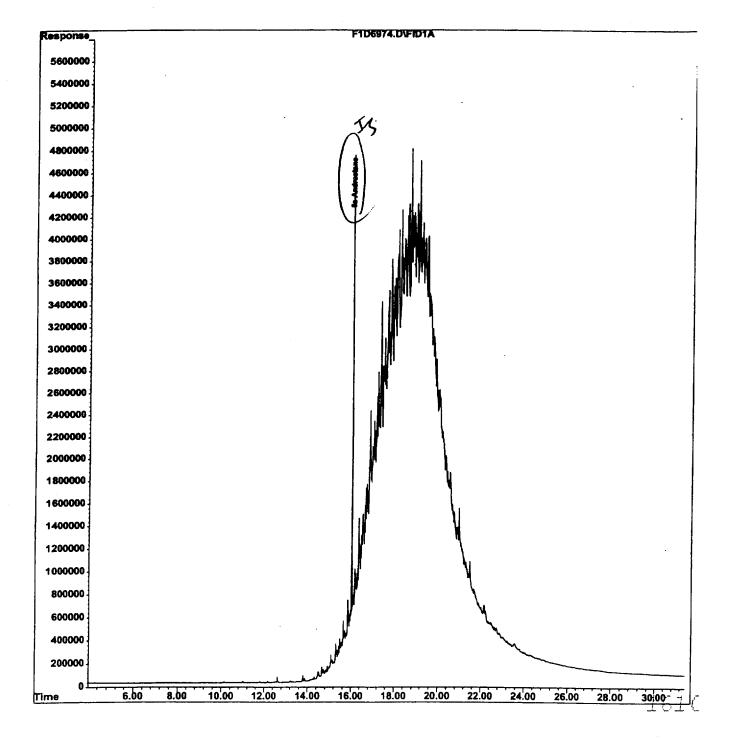
Acquired : 8-20-04 10:29:29 PM using AcqMethod ETPH-B.M

Instrument :

Sample Name: MOTOR OIL STAPPAGE

Misc Info : CITGO 10W-30

Vial Number: 2



File : C:\HPCHEM\1\DATA\AUG04\040819\F1D6976.D

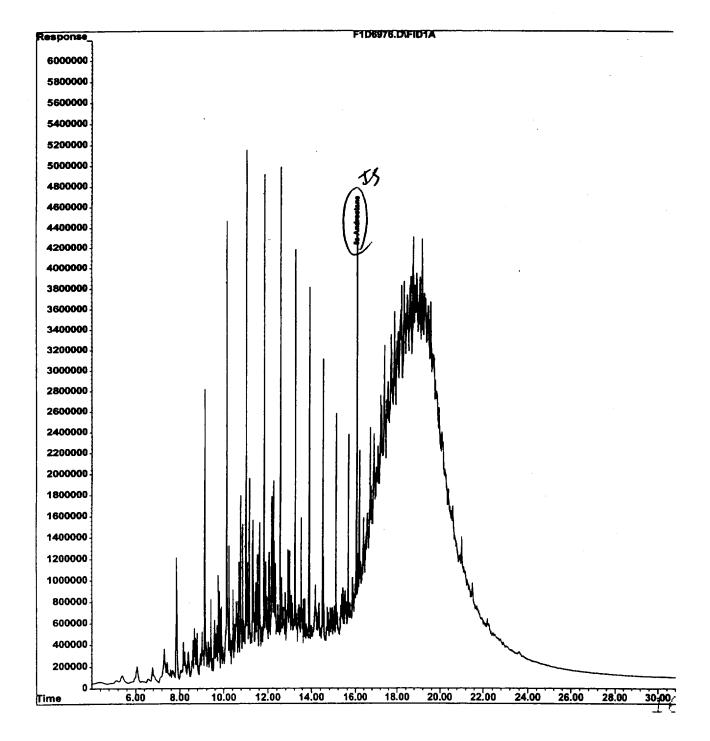
Operator : TT

Acquired : 8-20-04 11:56:45 PM using AcqMethod ETPH-B.M

Instrument : F1

Sample Name: MOTOR OIL + DIESEL STATES

Misc Info : Vial Number: 3



# APPENDIX B LNAPL VOLUME CALCULATIONS – BACKUP INFORMATION

# CALCULATION OF SITE-SPECIFIC LNAPL VOLUMES SUMMARY OF INPUT PARAMETERS

Since sand is the dominant lithology, an average sand lithology was selected. Other data were considered and the following input data were utilized in the site-specific LNAPL calculations:

- Effective Porosity 0.30, consistent with site soil types
- Hydraulic conductivity 6.4 ft/day, average of geometric means of the three soil types
- van Genuchten alpha average sand value from API and average value based on range of conductivities
- van Genuchten n same as for alpha
- Residual water saturation same as for alpha
- Surface tension average of the 5 observed LNAPL types from API reference tables
- Interfacial tension average of the 5 observed LNAPL types from API reference tables
- Dynamic viscosity average of 9 values for "oil" from July 2004 LNAPL analyses
- Specific gravity average of 9 values for "oil" from July 2004 LNAPL analyses

# **CALCULATION OF SITE-SPECIFIC LNAPL VOLUMES**

## **EQUATIONS USED**

All equations below are calculated as a function elevation (z)

Weight-height equivalent pressure head for water-phase	h <sub>w</sub> (z)=z <sub>aw</sub> -z
Water-height equivalent pressure for oil phase	h <sub>0</sub> (z)=p <sub>ro</sub> *(z <sub>ao</sub> -z)
Air-oil phase capillary head	h <sub>ao</sub> (z)=ρ <sub>ro</sub> *(z-z <sub>ao</sub> )
Oil-water phase capillary head	h <sub>ow(</sub> z)=h <sub>o</sub> (z)-h <sub>w</sub> (z)
van Genuchten parametric model for 2- and 3-phase saturation-pressure relation	Sstar(h)= if[h>0, [(1+(a*h)^n)^-m,1]
Effective water-phase saturation	$Sbar_{w}(z) = Sstar(\beta_{ow}^{*}h_{ow}(z))$
Water-phase saturation	$S_w(z)=S_m+(1-S_m)^*Sbar_w(z)$
Effective total liquid saturation	Sbar <sub>t</sub> (z)= Sstar(β <sub>ow</sub> *h <sub>ow(</sub> z))
Oil phase saturation (calculated in 2 steps to account for negative values)	Stemp <sub>0</sub> (z)=S <sub>m</sub> _S <sub>w</sub> (z)+(1-S <sub>m</sub> )*Sbar <sub>1</sub> (z)
	k <sub>temp</sub> (z)=((Sbar <sub>t</sub> (z)-Sbar <sub>w</sub> (z))^.5)*[(1- Sbar <sub>w</sub> (z)^(1/m))^m-(1-Sbar <sub>t</sub> (z)^(1/m))^m]^2
Upper limit for integration of NAPL volume (assumed to be air-oil interface)	z <sub>u</sub> =z <sub>ow</sub> +D <sub>0</sub>
Indefinite integral equation for NAPL volume	$V(z)=\int \Phi^*S_0(z) dz$
NAPL volume in soil	V <sub>o</sub> =V(z <sub>u</sub> )-V(z <sub>ow</sub> )
Relative permability of NAPL (step 1)	$k_{ro}(z)=if(Sbar_{l}(z) > Sbar_{w}(z), k_{temp}(z),0)$
Indefinite integral equation for the relative permability of NAPL	$K_{ro}(z) = \int k_{ro}(z) dz$
Relative permability of NAPL	$Kro=[1/(z_{u}^{-}z_{ow})]^{*}(K_{ro}(z_{u})-K_{ro}(z_{ow}))$
	· · · · · · · · · · · · · · · · · · ·

SO(z)=if(Stemp0 > 0, Stemp0(z), 0)

#### Source of Equations used:

Source: "Estimation of Free Hydrocarbon Volume From Fluid Levels in Monitoring Wells", by R.J. Lenhard and J.C. Parker, Ground Water, 28(1), 1990

### Soil Parameters

Effective Porosity (Φ)	
Hydraulic conductivity (k <sub>w</sub> ) (ft/day)	
van Genuchten parameter, a (1/ft)	
van Genuchten parameter, n	
Residual water saturation (S <sub>m</sub> )	· Victory
Irreducible Water Content (8 <sub>wr</sub> )	

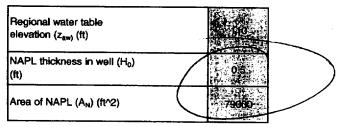
## General constants

Surface tension of uncontaminated water ( $\sigma_{aw}$ ) (dyne/cm)	
Water Density (ρ <sub>w</sub> ) (lb/ft^3)	
Dynamic viscosity of water (μ <sub>w</sub> ) (poise)	
Acceleration due to gravity (g) (ft/s^2)	

### **LNAPL** Parameters

Surface Tension (σ <sub>ao</sub> ) (dyn/cm)	
Interfacial Tension ( $\sigma_{ow}$ ) (dyn/cm)	
Dynamic Viscosity (µ <sub>0</sub> ) (P)	0.7282
Specific Gravity (pro)	0.8718

### **Operational Data**



### **NOTE**

To calculate results, press enter, and then press Ctrl-n. The spreadsheet does not automatically calculate the results.

Parameter	<u>Equation</u>	Resulf
Van Genuchten parameter m	m = 1 - 1/n	987
NAPL density (p <sub>0</sub> ) (lb/ft^3)	$\rho_0 = \rho_{ro}^* \rho_w$	54.400
Scaling coefficient air-oil (β <sub>80</sub> )	$\beta_{ao} = \sigma_{aw}/\sigma_{ao}$	2.681
Scaling coefficient oil-water (β <sub>ow</sub> )	$\beta_{ow} = \sigma_{aw}/\sigma_{ow}$	1,514,437,5
Residual water saturation (S <sub>m</sub> )	S <sub>m</sub> =6 <sub>w</sub> / Φ	0.150
Elevation of air-oil interface (z <sub>ao</sub> ) (ft)	Z <sub>eo</sub> =H <sub>0</sub> +Z <sub>ow</sub>	110.064
Elevation of oil-water interface (z <sub>ow</sub> ) (ft)	z <sub>ow</sub> =z <sub>ew</sub> -H₀*ρ <sub>ro</sub>	109,584
NAPL thickness in soil (D <sub>0</sub> ) (ft)	$D_0 = (\rho_{ro}^* \beta_{ao}^* H_0) / (\beta_{ao}^* \rho_{ro}^* \beta_{ow} (1 - \rho_{ro}))$	
Specific volume of NAPL in soil (V <sub>0</sub> ) (ft^3/ft^2)	See included equations	
NAPL volume in soil (V) (ft^3)	V = V <sub>0</sub> *A <sub>N</sub>	208.63
NAPL volume in soil (V) (Gal)	7.48 Gal / ft^3	
Permeability of NAPL relative to water	See included equations	25754E-03

### Soil Parameters

Effective Porosity (Φ)	
Hydraulic conductivity (k <sub>w</sub> ) (ft/day)	
van Genuchten parameter, α (1/ft)	
van Genuchten parameter, n	2.680 fr
Residual water saturation (S <sub>m</sub> )	: apriste :
Irreducible Water Content (0 <sub>wr</sub> )	

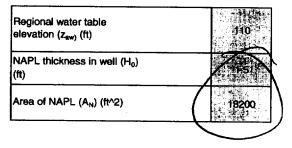
### **LNAPL** Parameters

Surface Tension (σ <sub>ao</sub> ) (dyn/cm)	27.15
Interfacial Tension ( $\sigma_{ow}$ ) (dyn/cm)	48-17
Dynamic Viscosity (μ <sub>0</sub> ) (P)	0,7262
Specific Gravity (pro)	e oznaby.

### General constants

Surface tension of uncontaminated water ( $\sigma_{aw}$ ) (dyne/cm)	
Water Density (ρ <sub>w</sub> ) (lb/ft^3)	
Dynamic viscosity of water $(\mu_w)$ (poise)	2001 H
Acceleration due to gravity (g) (ft/s^2)	174.

### **Operational Data**



### NOTE

To calculate results, press enter, and then press Ctrl-n. The spreadsheet does **not** automatically calculate the results.

<u>Parameter</u>	Equation	Result
Van Genuchten parameter m	m = 1 - 1/n	0.627
NAPL density (p <sub>0</sub> ) (lb/ft^3)	ρ <sub>0</sub> =ρ <sub>10</sub> °ρ <sub>w</sub>	54 400
Scaling coefficient air-oil (β <sub>so</sub> )	$\beta_{ao} = \sigma_{aw}/\sigma_{ao}$	12.681
Scaling coefficient oil-water (β <sub>ow</sub> )	$\beta_{ow} = \sigma_{ew}/\sigma_{ow}$	<b>1614</b>
Residual water saturation (S <sub>m</sub> )	S <sub>m</sub> ≖θ <sub>wr</sub> / Φ	0.150
Elevation of air-oil interface (z <sub>eo</sub> ) (ft)	z <sub>eo</sub> =H <sub>0</sub> +z <sub>ow</sub>	110.192
Elevation of oil-water interface (z <sub>ow</sub> ) (ft)	z <sub>ow</sub> =z <sub>aw</sub> -H <sub>o</sub> *p <sub>ro</sub>	08,692
NAPL thickness in soil (D <sub>0</sub> ) (ft)	$D_0 = (\rho_{ro} * \beta_{ao} * H_0) / (\beta_{ao} * \rho_{ro} * \beta_{ow} (1 - \rho_{ro}))$	
Specific volume of NAPL in soil (V <sub>0</sub> ) (ft^3/ft^2)	See included equations	
NAPL volume in soil (V) (ft^3)	V = V <sub>0</sub> *A <sub>N</sub>	7488.24
NAPL volume in soil (V) (Gal)	7.48 Gal / ft^3	
Permeability of NAPL relative to water	See included equations	1.2226E-01



### **Soil Parameters**

Effective Porosity (Φ)	
Hydraulic conductivity (k <sub>w</sub> ) (ft/day)	
van Genuchten parameter, α (1/ft)	18 100 H
van Genuchten parameter, n	2,680
Residual water saturation (S <sub>m</sub> )	// 40h 5000
Irreducible Water Content (0 <sub>w</sub> )	

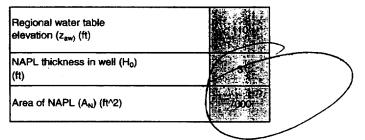
### **LNAPL Parameters**

Surface Tension ( $\sigma_{so}$ ) (dyn/cm)	
Interfacial Tension ( $\sigma_{ow}$ ) (dyn/cm)	4877
Dynamic Viscosity (μ <sub>0</sub> ) (P)	0.7262
Specific Gravity (pro)	<sup>‡</sup> 40. <b>8718</b> ;√

### General constants

Surface tension of uncontaminated water (σ <sub>aw</sub> ) (dyne/cm)	
Water Density (p <sub>w</sub> ) (lb/ft^3)	1824
Dynamic viscosity of water (μ <sub>w</sub> ) (polse)	Poor it
Acceleration due to gravity (g) (ft/s^2)	32 174

### **Operational Data**



### **NOTE**

To calculate results, press enter, and then press Ctrl-n. The spreadsheet does **not** automatically calculate the results.

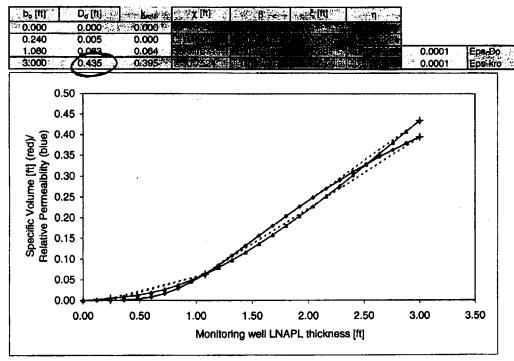
<u>Parameter</u>	<u>Equation</u>	Result
Van Genuchten parameter m	m = 1 - 1/n	0.627
NAPL density (ρ <sub>0</sub> ) (lb/ft^3)	ρ <sub>0</sub> =ρ <sub>го</sub> *ρ <sub>₩</sub>	54:400
Scaling coefficient air-oil (β <sub>aα</sub> )	$\beta_{ao} = \sigma_{aw}/\sigma_{ao}$	2.681
Scaling coefficient oil-water (β <sub>ow</sub> )	$\beta_{ow} = \sigma_{ew}/\sigma_{ow}$	5.514
Residual water saturation (S <sub>m</sub> )	S <sub>m</sub> =θ <sub>wr</sub> / Φ	0.150
Elevation of air-oil interface (z <sub>ac</sub> ) (ft)	z <sub>eo</sub> =H <sub>0</sub> +z <sub>ow</sub>	# \$110.385
Elevation of oil-water interface (z <sub>ow</sub> ) (ft)	z <sub>ow</sub> =z <sub>aw</sub> -H <sub>0</sub> *ρ <sub>ro</sub>	107,385
NAPL thickness in soil (D <sub>0</sub> ) (ft)	$D_0 = (\rho_{ro} * \beta_{ao} * H_0) / (\beta_{ao} * \rho_{ro} * \beta_{ow} (1 - \rho_{ro}))$	
Specific volume of NAPL in soil (V <sub>0</sub> ) (ff^3/ff^2)	See included equations	
NAPL volume in soil (V) (ft^3)	V = V <sub>0</sub> *A <sub>N</sub>	2493-801
NAPL volume in soil (V) (Gal)	7.48 Gal / ft^3	Part of the second
Permeability of NAPL relative to water	See included equations	3.7104E-01

# API Model

Maximum Monit	toring Well		Calculated Parameters
LNAPL Thickne	ss [feet]		Van Genuchten "M"
b <sub>o</sub> =	3.000		$\alpha_{no} = 3.836$ air/LNAPL " $\alpha$ " [ft.1]
		_	0.854   LNAPL/water "α" [ft <sup>-1</sup> ]
Soil Characteris	rtic		Z <sub>ao</sub> = 0.385 elevation of air-LNAPL interface [ft]
N=	0.300	porosity	Zow = 2.615 elevation of LNAPL-water interface [1
N =	2.680	van Genuchten "N"	Z <sub>max</sub> = 1.245 maximum free-product elevation [ft]
α =	4.400	van Genuchten "α" (ft <sup>-1</sup> )	λ = 1.124 pore-size distribution index
S <sub>wr</sub> =	0.150	irreducible water saturation	Ψ <sub>b</sub> = 0.148 B-C displacement pressure head [ft]
S <sub>orv</sub> =	0.050	residual LNAPL saturation (vadose)	
S <sub>ors</sub> =	0.050	residual LNAPL saturation (saturated)	
			Set Tools > Option > Calculations tab to "Manual."
Fluid Character	istics:	7.	Press Ctrl+Shift+S to calculate sheet
ρ <sub>o</sub> =	0.872	LNAPL density [gm/cc]	
σ <sub>aw</sub> =	72.800	air/water surface tension [dyne/cm]	
$\sigma_{ao} =$	72.800	air/LNAPL surface tension [dyne/cm]	
σ <sub>ow</sub> =	48,100	LNAPL/water surface tension [dyne/cm]	

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Specific Volume = 0.435 ft3/ft2

Napl in Soil =

0.435 ft3

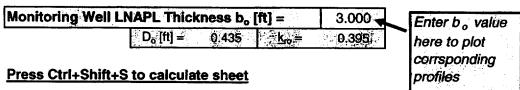
T+2

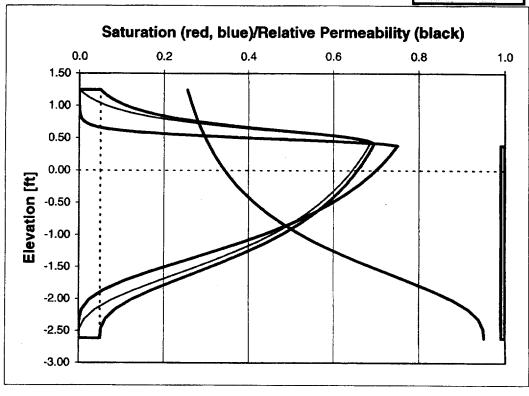
X 7000 ft2 = 3045 ft3

3045 ft3 = 22,778 gallows

\* Lenhard-Parker, basis of my LNAPL Volume calculations, Determines 18,653 gellons N 18% Difference

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#### Soil Parameters

F-0300
E 105 8
1 701142

#### **LNAPL Parameters**

Surface Tension (σ <sub>ao</sub> ) (dyn/cm)	
Interfacial Tension (σ <sub>ow</sub> ) (dyn/cm)	48 C
Dynamic Viscosity (μ <sub>0</sub> ) (P)	
Specific Gravity (pro)	7703711

### General constants

Surface tension of uncontaminated water ( $\sigma_{ew}$ ) (dyne/cm)	28 43
Water Density (p <sub>w</sub> ) (lb/ft^3)	
Dynamic viscosity of water (μ <sub>w</sub> ) (poise)	COL :
Acceleration due to gravity (g) (ft/s/2)	7143 THE 1

### **Operational Data**

Regional water table elevation (z <sub>ew)</sub> (ft)	
NAPL thickness in well (H <sub>0</sub> ) (ft)	
Area of NAPL (A <sub>N</sub> ) (ft^2)	7000

### NOTE

To calculate results, press enter, and then press Ctrl-n. The spreadsheet does not automatically calculate the results.

Beede - Average van & parameters from Conductivity Ranger From API Database

<u>Parameter</u>	<u>Equation</u>	Result
Van Genuchten parameter m	m = 1 - 1/n	0.476
NAPL density (ρ <sub>0</sub> ) (lb/ft^3)	$\rho_0 = \rho_{ro}^* \rho_w$	54,400
Scaling coefficient air-oil (β <sub>ao</sub> )	$\beta_{ao} = \sigma_{aw}/\sigma_{ao}$	2.68T
Scaling coefficient oil-water (β <sub>ow</sub> )	$\beta_{cw} = \sigma_{nw}/\sigma_{cw}$	1.514
Residual water saturation (S <sub>m</sub> )	S <sub>m</sub> =θ <sub>wr</sub> / Φ	0.379
Elevation of air-oil interface (z <sub>ao</sub> ) (ft)	z <sub>ac</sub> =H <sub>0</sub> +z <sub>cw</sub>	.110.385
Elevation of oil-water interface (z <sub>ow</sub> ) (ft)	z <sub>ow</sub> =z <sub>ew</sub> -H <sub>0</sub> *ρ <sub>ro</sub>	#15 - 107.385
NAPL thickness in soil (D <sub>0</sub> ) (ft)	$D_0 = (\rho_{ro}^* \beta_{ao}^* H_0) / (\beta_{ao}^* \rho_{ro}^- \beta_{ow} (1 - \rho_{ro}))$	
Specific volume of NAPL in soil (V <sub>0</sub> ) (ft/3/ft/2)	See included equations	and the second s
NAPL volume in soil (V) (ft^3)	V = V <sub>0</sub> *A <sub>N</sub>	84.81
NAPL volume in soil (V) (Gal)	7.48 Gal / ft^3	•
Permeability of NAPL relative to water	See included equations	7.5173E-03